

If you have an affected existing or new pitch working tank, you must duct the exhaust from the tank to either the coking oven control device, the defumer control device, or an equivalent thermal or catalytic oxidizer.

If you have an affected existing or new chromium refractory products kiln or an affected existing clay refractory products kiln, you must use natural gas, or an equivalent fuel, as the kiln fuel at all times except during periods of natural gas curtailment or other periods when natural gas is not available.

F. What Are the Testing and Initial Compliance Requirements for Sources Subject to Emission Limits?

Under today's final rule, you must conduct an initial performance test on each affected source to demonstrate initial compliance with the emission limits. In accordance with 40 CFR 63.7(a)(2), you are required to conduct the test within 180 days after the compliance date using specified test methods.

If you have an affected existing or new shape dryer, curing oven, kiln, coking oven, or defumer, or a new shape preheater, and you choose to comply with the THC concentration limit of 20 ppmvd corrected to 18 percent oxygen, you must measure emissions of THC in stack gases exhausted to the atmosphere using EPA Method 25A of 40 CFR part 60, appendix A, Determination of Total Gaseous Organic Concentration Using a Flame Ionization Analyzer. You must also measure the oxygen concentration of the stack gas using EPA Method 3A of 40 CFR part 60, appendix A, Determination of Oxygen and Carbon Dioxide Concentrations in Emissions From Stationary Sources (Instrumental Analyzer Procedure). If you decide to comply with the 95 percent THC reduction limit, you must measure THC mass emissions at the inlet and outlet of the control device using EPA Method 25A.

For continuous process sources, you must conduct a minimum of three 1-hour test runs. For batch process sources, you must conduct at least two test runs. Each batch process test run must be conducted over a separate batch cycle, unless you manufacture the product associated with the maximum organic HAP processing rate infrequently and it will disrupt production to perform the compliance test over multiple process cycles. In such cases, you may conduct both runs of the performance test simultaneously over a single batch process cycle using paired sampling trains.

Today's final rule requires affected batch process sources to be tested

throughout two complete batch cycles unless you develop an emissions profile or meet certain conditions for terminating a performance test run before the completion of the batch cycle. If you choose to develop an emissions profile, you must sample THC emissions throughout a complete batch cycle, determine the average THC mass emissions rate for each hour of the batch cycle, and identify the 3-hour period of peak THC emissions. During any subsequent test runs, you are not required to sample emissions outside that 3-hour period of peak THC emissions. During subsequent performance tests, you will have to complete at least two test runs, but you will only have to test during the 3-hour peak emissions period for each run.

If you choose not to develop an emissions profile, you may terminate testing before the completion of a batch cycle if you meet certain conditions. For each of two test runs, you will have to begin testing at the start of the batch cycle and continue testing for at least 3 hours beyond the precise time when the process reaches peak operating temperature. You may stop the test run at that time if you can show that the following conditions are met: (1) THC concentrations are not increasing over the 3-hour period since the process peak temperature was reached; (2) at least 1 hour has passed since any reduction in the operating temperature of the control device (thermal or catalytic oxidizer); and (3) either the average THC concentration at the inlet to the control device for the previous hour has not exceeded 20 ppmvd, corrected to 18 percent oxygen, or your source met the applicable emission limit at the control device outlet during each of the previous 3 hours after the process reached peak temperature.

For both continuous process and batch process performance tests, you must conduct performance tests on affected thermal process sources under the conditions that will result in the highest levels of organic HAP emissions expected to occur for that affected source. You determine these "worst-case" conditions by taking into account the organic HAP processing rate, the process operating temperatures, and the processing times. The organic HAP processing rate is the rate at which the mass of organic HAP materials contained in refractory shapes are processed in an affected thermal process source.

If you decide to start production of a refractory product that is likely to have an organic HAP processing rate that is more than 10 percent greater than the rate established during the most recent

performance test, you will be required to conduct a new performance test for that product and establish a new operating limit for the organic HAP processing rate. You will also have to conduct a new performance test on an affected uncontrolled kiln following any process changes that are likely to increase kiln emissions of organic HAP.

If the source is a batch process source and is controlled with a thermal or catalytic oxidizer, you may reduce the operating temperature of the control device or shut the control device off if you satisfy all of the following conditions: (1) You do not use an emissions profile and limit testing to the 3-hour peak emissions period; (2) at least 3 hours have passed since the process unit reached its maximum temperature; (3) the applicable emission limit (THC concentration or THC percentage reduction) has been met during each of the three 1-hour periods since the process reached peak temperature; (4) mass emissions of THC have not increased during the 3-hour period since maximum process temperature was reached; and (5) either the average THC concentration at the inlet to the oxidizer has not exceeded 20 ppmvd, corrected to 18 percent oxygen, for at least 1 hour, or the applicable emission limit has been met during each of the four 15-minute periods immediately following the oxidizer temperature reduction. If you elect to shut off or reduce the temperature of a thermal or catalytic oxidizer by satisfying these conditions, you may use the results from the performance test to establish the time at which the oxidizer for that specific source can be shut off (or temperature reduced) during the production of other refractory products that use organic HAP. For any such product, you must operate the oxidizer at a temperature at least as high as that established during the performance test, minus 16°C (25°F), from the start of the batch cycle until 3 hours have passed since the process reached its peak temperature. You will have to maintain that oxidizer temperature for the same length of time beyond the process peak temperature as during the performance test.

For each new kiln that manufactures clay refractory products, you must measure emissions of HF and HCl using one of three methods: (1) EPA Method 26A of 40 CFR part 60, appendix A, Determination of Hydrogen Halide and Halogen Emissions from Stationary Sources—Isokinetic Method; (2) EPA Method 26 of 40 CFR part 60, appendix A, Determination of Hydrogen Halide and Halogen Emissions from Stationary Sources—Non-isokinetic Method; or (3)