

TABLE 2.—EMISSION LIMITS FOR NEW OR RECONSTRUCTED AFFECTED SOURCES—Continued

| If you apply surface coatings to metal cans or metal can parts in this subcategory . . . | For all coatings of this type . . . | Then, you must meet the following organic HAP emission limit in kilograms (kg) HAP/liter solids (lb HAP/gal solids): ^{1,2} |
|--|---|---|
| 4. End coating | c. Nonaseptic side seam stripes on food cans d. Side seam stripes on general line nonfood cans. e. Side seam stripes on aerosol cans a. Aseptic end seal compounds b. Nonaseptic end seal compounds c. Repair sprays | 0.72 (5.96). 1.18 (9.84). 1.46 (12.14). 0.06 (0.54). 0.00 (0.00). 0.64 (5.34). |

¹ If you apply surface coatings of more than one type within any one subcategory, you may calculate an overall subcategory emission limit according to 40 CFR 63.3531(i).

² Rounding differences in specific emission limits are attributable to unit conversions.

TABLE 3.—EMISSION LIMITS FOR EXISTING AFFECTED SOURCES

| If you apply surface coatings to metal cans or metal can parts in this subcategory . . . | For all coatings of this type . . . | Then, you must meet the following organic HAP emission limit in kg HAP/liter solids (lb HAP/gal solids): ^{1,2} |
|--|--|---|
| 1. One- and two-piece D&I can body coating | a. Two-piece beverage cans—all coatings | 0.07 (0.59). |
| | b. Two-piece food cans—all coatings | 0.06 (0.51). |
| | c. One-piece aerosol cans—all coatings | 0.12 (0.99). |
| 2. Sheetcoating | Sheetcoating | 0.03 (0.26). |
| 3. Three-piece can assembly | a. Inside spray | 0.29 (2.43). |
| | b. Aseptic side seam stripes on food cans | 1.94 (16.16). |
| | c. Nonaseptic side seam stripes on food cans | 0.79 (6.57). |
| | d. Side seam stripes on general line nonfood cans. | 1.18 (9.84). |
| | e. Side seam stripes on aerosol cans | 1.46 (12.14). |
| 4. End coating | a. Aseptic end seal compounds | 0.06 (0.54). |
| | b. Nonaseptic end seal compounds | 0.00 (0.00). |
| | c. Repair sprays | 2.06 (17.17). |

¹ If you apply surface coatings of more than one type within any one subcategory, you may calculate an overall subcategory emission limit according to 40 CFR 63.3531(i).

² Rounding differences in specific emission limits are attributable to unit conversions.

TABLE 4.—EMISSION LIMITS FOR AFFECTED SOURCES USING THE CONTROL EFFICIENCY/OUTLET CONCENTRATION COMPLIANCE OPTION

| If you use the control efficiency/outlet concentration option to comply with the emission limitations for any coating operation(s) . . . | Then you must comply with one of the following by using an emissions control system to . . . |
|--|--|
| 1. In a new or reconstructed affected source | a. Reduce emissions of total HAP, measured as total hydrocarbons (THC) (as carbon), ¹ by 97 percent; or b. Limit emissions of total HAP, measured as THC (as carbon) ¹ to 20 parts per million by volume, dry (ppmvd) at the control device outlet and use a permanent total enclosure. |
| 2. In an existing affected source | a. Reduce emissions of total HAP, measured as THC (as carbon), ¹ by 95 percent; or b. Limit emissions of total HAP, measured as THC (as carbon) ¹ to 20 ppmvd at the control device outlet and use a permanent total enclosure. |

¹ You may choose to subtract methane from THC as carbon measurements.

Operating Limits. If you reduce emissions by using a capture system and add-on control device (other than a solvent recovery system for which you conduct a liquid-liquid material balance), the operating limits apply to you. These limits are site-specific parameter limits you determine during the initial performance test of the system. For capture systems that are not permanent total enclosures (PTE), you must establish average volumetric flow rates or duct static pressure limits for

each capture device (or enclosure) in each capture system. For capture systems that are PTE, you must establish limits on average facial velocity or pressure drop across openings in the enclosure.

For thermal oxidizers, you must monitor the combustion temperature. For catalytic oxidizers, you must monitor the temperature immediately before and after the catalyst bed or you must monitor the temperature at the inlet to the catalyst bed and implement

a site-specific inspection and maintenance plan for the catalytic oxidizer. For carbon adsorbers for which you do not conduct a liquid-liquid material balance, you must monitor the carbon bed temperature and the amount of steam or nitrogen used to desorb the bed. For condensers, you must monitor the outlet gas temperature from the condenser. For concentrators, you must monitor the temperature of the desorption concentrate stream and the